Amendments to the Specification:

Please replace the paragraph beginning at page 1, line 17 with the following amended paragraph:

The invention provides particulate plant sterol compositions and methods for making the same. Particulate plant sterol compositions of the invention are useful for dispersion in aqueous media, including aqueous food and beverage products. When dispersed in aqueous media, such as a juice, the compositions do not impart gritty, chalky, or other undesirable ~~otherundesirable~~ sensory qualities (i.e. with respect to color, flavor, and mouthfeel~~mouth feel~~) to the aqueous media. Methods for preparing the compositions are also provided, including one-pass milling methods that avoid the need for size classification and recycling of undesirably sized particles.

Please replace the paragraph beginning at page 10, line 23 with the following amended paragraph:

Impact- or attrition-milling can be performed with a gap mill. Gap mills typically include a plurality of flat blades arranged around a conical-shaped rotor and a corresponding conical ribbed stator. Size reduction is accomplished in part by the impact of particles with the rotor and stator, but predominantly by particle-particle collisions. Typically, a rotor-stator gap is in the range of from about 0.025" to about 0.05". For example, in certain embodiments, the rotor-stator gap is about 0.03". The rotor speed is adjustable so that an average tip speed of from about 110 m/s to about 150 m/s is achieved. In certain embodiments, an average tip speed is from about 120 to about 135 m/s. Gap mills are available commercially from Microtec GmbH~~Microtec (e.g., Microtec Microtec Gap Mill)~~, Bauermeister, Inc. ~~(e.g., Bauermeister ASIMA mill)~~, ~~Netzsch~~ NETZSCH Fine Particle Technology, and ~~Hosokawa-Bepex~~ Hosokawa Bepex GmbH.

Please replace the paragraph beginning at page 11, line 10 with the following amended paragraph:

In another process for preparing a particulate plant sterol composition, a plant sterol starting material is milled in a jet- or vortex-mill. In these mills, the driving force for comminution is derived from the high volumetric flows of high pressure air or other gas, such as $N_2$, which will thereby produce an inert atmosphere for milling. Comminution is mainly by particle-particle collisions, and the heat generated in the process is absorbed by the gas cooling upon expansion from, for example, 5 to 6 bar to atmospheric pressure and dissipated by the high gas flow. Particle-particle forces result in fine comminution of the starting material, which does not exit until it has achieved a minimal particle size, according to the design of the chamber and the vortex. Vortex mills are available from SuperFine Ltd., INOX Ltd., and ~~Netzsch~~ NETZSCH Fine Particle Technology, or as described in U.S. Pat. No. 5,855,326.

Please replace the paragraph beginning at page 13, line 26 with the following amended paragraph:

5 kg of 2 mm diameter sterol pastilles (Cargill, Incorporated, 90% by weight a mixture of $\beta$-sitosterol, campesterol, stigmasterol, brassicasterol, campestanol, $\beta$-sitostanol, and $\Delta$-5-avenosterol) were melted in a Parr® reactor and forced under a N2(g) pressure of 35 psig into a Spraying Systems, Inc. SU-42 two-fluid nozzle at a rate of 2.7 gph, with the second, atomizing fluid being 3.6 scfm of 90 psig air; the fluid temperatures were 375 °F. The product was collected in a conical chamber under atmospheric pressure and ambient temperature. Particle size analysis on a Horiba® LA-910 Particle Size Analyzer [See Table I, SP-1] showed the sterols to have 6 volume-% (as determined on a volume-weighted PSD) and 56 surface-area%- (as determined on a surface-area weighted PSD) in the "fines" region (particles less than 2 microns in diameter), with the "fines" peak mean diameter being 0.6 microns or greater. The calculated specific area of the overall material was 1.1 m2/g.

Please replace the paragraph beginning at page 14, line 11 with the following amended paragraph:

Sterol pastilles (as described above) 2 mm in diameter were cooled in-line to an inlet temperature of about –175 °F before entering a Microtec® Model 200 "Gap" Mill with a 0.030" gap. The pre-cooled sterol pastilles were milled in a single pass at a feed rate of about 465 #/hr and a rotor speed of 12,000 rpm. The mill discharge temperature was –45 to –50 °F. The product was analyzed on a Horiba® LA-910 Particle Size Analyzer. [See Table I, CG-79] ~~See Table I.~~

Please replace the paragraph beginning at page 14, line 20 with the following amended paragraph:

Sterol pastilles (as described above) 2 mm in diameter were cooled in-line to an inlet temperature of about –245 °F before entering a Microtec® Model 200 "Gap" Mill with a 0.030" gap. The pre-cooled sterol pastilles were milled in a single pass at a feed rate of about 630 #/hr and a rotor speed of 12,000 rpm. The mill discharge temperature was –75 °F. The product was analyzed on a Horiba® LA-910 Particle Size Analyzer (see Example 8). [See Table I, CG-56] ~~See Table I.~~

Please replace the paragraph beginning at page 14, line 27 with the following amended paragraph:

Sterol pastilles (as described above) 2 mm in diameter were cooled in-line to an inlet temperature of about –225 °F before entering a Microtec® Model 200 "Gap" Mill with a 0.030" gap. The pre-cooled sterol pastilles were milled in a single pass at a feed rate of about 500-550 #/hr and a rotor speed of 12,000 rpm. Single pass milling was performed for about 3.5 hr total (1700# of sterol pastilles). The product was analyzed on a Horiba® LA-910 Particle Size Analyzer. The mill discharge temperature was –75 °F. [See Table I, CG-522] ~~See Table I.~~

Please replace the paragraph beginning at page 15, line 5 with the following amended paragraph:

Sterol pastilles (as described above) 2 mm in diameter were drawn at a rate of about 4 kg/hr into a 6"D SuperFine, Ltd. Vortex Mill with no cooling of the material. The driving force for the mill was an inlet stream of air at a pressure of about 5.5 bar. The product was analyzed on a Horiba® LA-910 Particle Size Analyzer. [See Table I, SF-1] ~~See Table I.~~

Please replace the paragraph beginning at page 15, line 15 with the following amended paragraph:

Samples SP-1, CG-79, CG-56, CG-522, and SF-1 were analyzed on a Horiba® LA-910 Particle Size Analyzer and the distribution of particles plotted as either volume (or mass)-weighted PSD vs. particle diameter or surface area-weighted PSD vs. particle diameter. Each composition's total specific surface area was also calculated from the particle size distribution. Results are set forth in Table I below.

Please replace Table I at pages 15-16 with the following amended Table I:

**Table I**

| | SP-1 | CG-79 | CG-56 | CG-522 | SF-1 |
|---|---|---|---|---|---|
| "Fines" Peak only, Volume-Weighted PSD - % of Total | 6 | 13.1 | 18.3 | 19 | 30 |
| "Fines" Peak only, Surface Area-Weighted PSD - % of Total | 56 | 75 | 79 | 83 | 85 |
| "Fines" Peak only, Surface Area-Weighted PSD - Mean Diameter [$\mu$] | 0.6 | 0.6 | 0.5 | 0.4 | 0.4 |
| Specific Surface Area Total Distribution – calculated from PSD [$m^2/g$] | 1.1 | 2.0 | 2.9 | 4.4 | 6.1 |
| Volume-Weighted PSD - % of Material > 35 $\mu$ in diameter | 3.7 | 9.4 | 0 | 0.3 | 0 |